

[CONTRIBUTION FROM THE BUREAU OF CHEMISTRY AND SOILS]

The Solubility in Liquid Ammonia of Hydrogen at 0° and of Nitrogen at 0, 50, 75, 90 and 100° at Pressures to 1000 Atmospheres. Critical Phenomena of Ammonia-Nitrogen Mixtures¹

By R. WIEBE AND V. L. GADDY

This work is part of a program to determine the physical properties of substances important in the production of fertilizers, such as ammonia, nitrogen, hydrogen and their mixtures.^{2,3} The

atmospheres. The results for hydrogen are given in Table I and Figs. 1 and 2. The points in Figs. 1 and 2 for the temperatures 25, 50, 75 and 100° have been included from a previous publication³ to show the marked difference in the behavior of hydrogen and nitrogen in liquid ammonia in the same range of pressure and temperature.

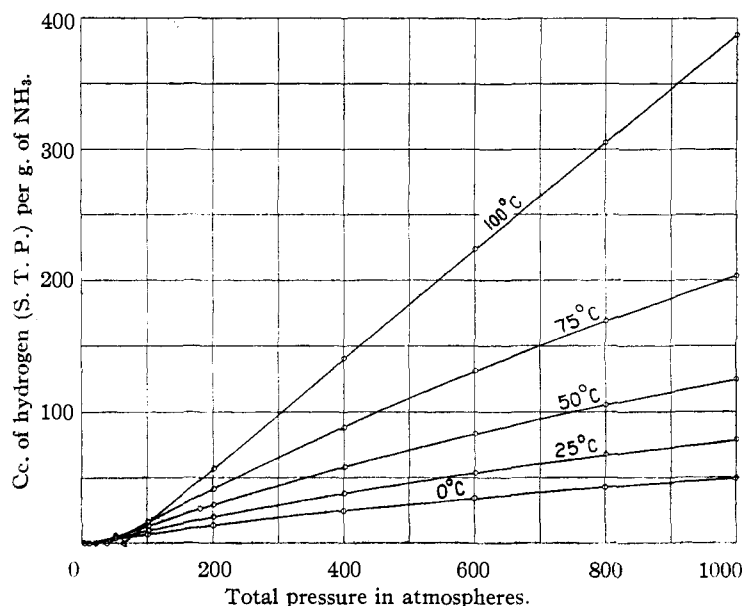


Fig. 1.—Solubility of hydrogen in liquid ammonia.

apparatus and method have been described previously. Pressures are given in international

that temperature.

TABLE I
THE SOLUBILITY OF HYDROGEN IN LIQUID AMMONIA AT 0°
Cc. of hydrogen at S. T. P. per g. of ammonia

Pressure, atm.	Number of runs	Solubility
50		(3.28) ^a
100	7	6.70
200	10	13.11
300		(18.96)
400	9	24.33
500		(29.27)
600	10	33.99
700		(38.25)
800	9	42.33
900		(46.20)
1000	8	49.77

^a Figures in parentheses are interpolated values.

(1) Read at the meeting of the American Chemical Society, Rochester, N. Y., September 6 to 10, 1937.

(2) Larson and Black, *Ind. Eng. Chem.*, **17**, 715 (1925).

(3) Wiebe and Tremearne, *THIS JOURNAL*, **55**, 975 (1933); **56**, 2357 (1934); **57**, 2601 (1935).

TABLE II
THE SOLUBILITY OF NITROGEN IN LIQUID AMMONIA
EXPERIMENTAL RESULTS
Cc of nitrogen at S. T. P. per g. of ammonia

P, atm.	0°		50°		75°		90°		100°	
	No. of runs	Soly. runs	No. of runs	Soly. runs	No. of runs	Soly. runs	No. of runs	Soly. runs	No. of runs	Soly. runs
50			5	6.63						
100	7	7.90	6	17.19	2	21.38			7	20.50
200	6	13.73	8	36.24	3	55.48			6	86.32
300									6	193.16
325									4	235.95
350							4	165.50		
400	4	20.76	4	65.35	4	120.66				Single phase
500							4	310.63		
550							6	430.8		
600	6	24.95	7	84.78	4	177.95				
700										Single phase
800	11	28.06	7	97.20	4	218.99				
1000	11	29.69	7	104.59	4	241.75				

Table III gives interpolated values obtained graphically for different temperatures. The values, especially the higher ones, cannot claim a high degree of accuracy.

TABLE III
INTERPOLATED VALUES OF THE SOLUBILITY OF NITROGEN IN LIQUID AMMONIA
Cc. of nitrogen at S. T. P. per g. of ammonia

Total P, atm.	Temperature, °C.										
	0	10	20	30	40	50	60	70	80	90	100
50	4.10	4.55	5.45	5.85	6.30	6.63	6.35	5.20	2.7		
100	7.90	9.40	11.11	13.02	15.09	17.19	19.14	20.51	21.10	21.0	20.50
200	13.73	16.77	20.42	24.81	30.16	36.24	43.02	50.93	60.67	72.7	86.32
300	17.70	22.30	27.60	34.30	42.50	51.90	63.87	79.0	99.8	134.9	193.16
400	20.76	26.42	33.11	41.45	52.10	65.35	82.22	105.6	137.5	218.8	
500	23.00	29.50	37.20	46.85	59.45	76.07	98.05	129.4	197.0	310.6	
600	24.95	31.84	40.43	51.17	65.31	84.78	110.8	149.3			
700	26.60	33.87	43.07	54.75	70.35	91.70	120.4	165.1			
800	28.06	35.52	45.19	57.68	74.39	97.20	127.8	177.6			
900	29.00	36.75	46.95	59.95	77.35	101.25	133.6	186.7			
1000	29.69	37.93	48.53	62.02	79.89	104.59	138.8	194.3			

The measurements in the neighborhood of the critical curve are cumbersome both in the heterogeneous and homogeneous region. Shaking is not very effective. Constant temperature and pressure for long periods of time are essential for attaining equilibrium. The following example will

above sets is sufficiently constant and might have been mistaken for true equilibrium. The results of May 11 are slightly higher than the composition of the vapor phase on May 7. This is caused by the introduction of nitrogen to keep the pressure constant during sampling and by loss of

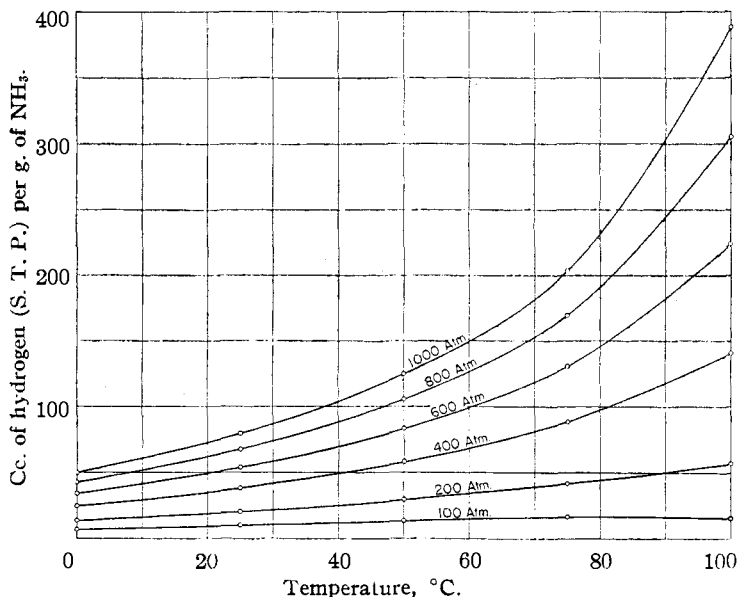


Fig. 2.—Solubility of hydrogen in ammonia.

illustrate some of the difficulties of knowing whether two phases or only a single phase was present. At 400 atmospheres total pressure and 100° results were obtained as follows. Any of the

liquid ammonia due to sampling itself. In order to make sure that enough ammonia was left to form a liquid phase, the pressure was reduced to 300 atmospheres at 100°. The following results were obtained

Time	COMPOSITION IN Cc. OF N ₂ AT S. T. P. PER G. OF NH ₃		
	Liquid phase		Vapor phase
April 29	312.8	313.9	
April 30	375.0	375.7	376.4
May 1	423.9	427.9	427.5
May 5	515.1	513.4	
May 6	553.2	553.9	551.9
May 7	561.8	566.1	591.7 590.4 596.5
May 11	599.3	600.9	599.6

Time	COMPOSITION IN Cc. OF N ₂ AT S. T. P. PER G. OF NH ₃	
	Liquid	Vapor
	197.55	836.9
	190.79	855.1
	190.38	855.9

Whether at 350 atmospheres a liquid phase was still present was not ascertained definitely.

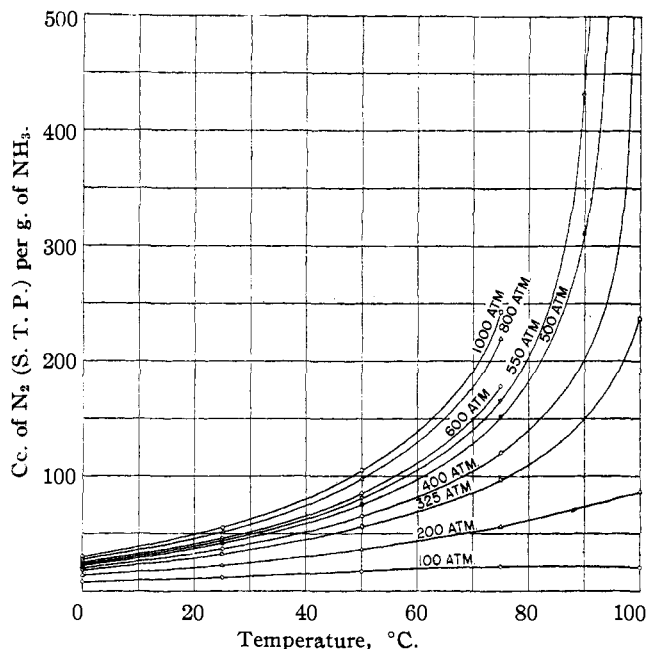


Fig. 3.—Solubility of nitrogen in ammonia, total pressure isobars.

From Figs. 3, 4 and 5 it can be seen that the critical pressure of the system ammonia-nitrogen at 90° is close to 600 atmospheres, while at 100° it has dropped to less than 400 atmospheres, thus rapidly approaching the critical point of pure liquid ammonia $p_c = 112.3$ atm., $t_c = 132.9^\circ$. The critical phenomena had not been anticipated at pressures so low as 600 atmospheres and 90° , or 400 atmospheres and 100° , but were instead ex-

pected in the neighborhood of 1000 atmospheres at 100° . At that pressure and temperature the densities of nitrogen and liquid ammonia are very nearly the same, and due to mutual solubility the densities would tend to approach each other even more rapidly, as proved to be true. The critical condition is recognized most readily in Fig. 5. Here the vapor pressure of ammonia forms the lower boundary. The dotted line indicates the

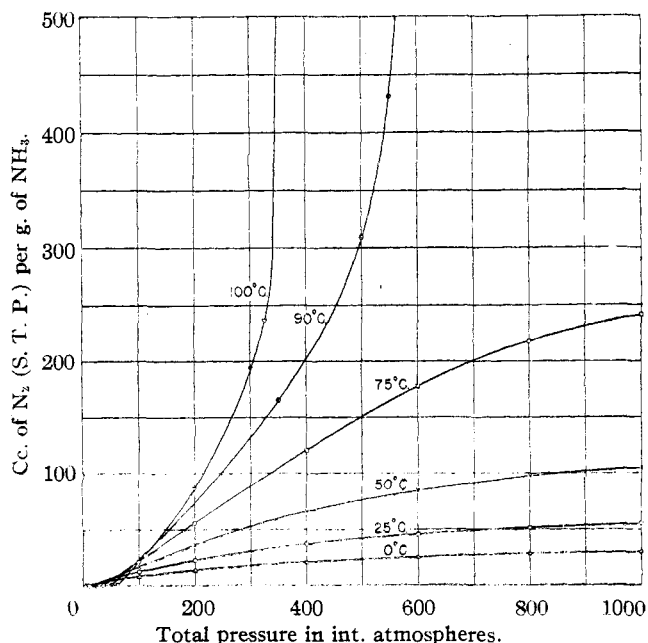


Fig. 4.—Solubility of nitrogen in ammonia.

probable trend of the critical curve of the mixture starting at the critical point of ammonia, rising to a very high pressure and finally curving back to end at the critical temperature $t_c = -147.1^\circ$ and pressure $p_c = 33.5$ atmospheres of nitrogen. A number of constant composition curves for the liquid phase have also been drawn, the numerical values of which are given in Table IV. The data were obtained graphically. For illustration the "200," "250" and "300" composition curves have been extrapolated roughly to show the possible trend of the vapor branch. These extrapolations are of course highly qualitative. The curves for the other compositions will likewise come down and make contact of the first order with the critical curve (envelope), in somewhat the fashion depicted. The shape of the curves seems to indicate retrograde condensation of the first kind.⁴

TABLE IV

TEMPERATURES AT CONSTANT COMPOSITION IN $^\circ\text{C}$.					
Pressure, atm.	Composition in cc. N_2 (S. T. P.) per g. liquid ammonia				
	100	150	200	250	300
325	76.4	90.4	96.6	100.6 ^a	
400	68.4	82.1	89.8	94.2 ^a	96.6 ^a
500	62.0	74.8	82.1	86.6	89.6
550	60.0	72.5	79.2	83.5	86.2
600		70.3			
800		65.3	72.9	77.5 ^a	
1000		63.0	70.8	75.5 ^a	

^a These values are rather uncertain.

Summary

The solubility of hydrogen in liquid ammonia

(4) For full discussion see, *e. g.*, Kuenen, "Theorie der Verdampfung und Verflüssigung von Gemischen," Joh. Ambrosius Barth, Leipzig, 1906.

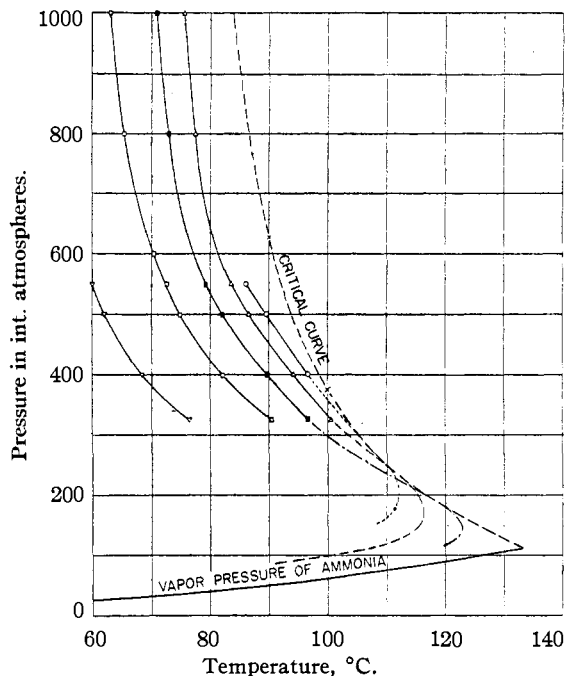


Fig. 5.—Constant composition curves and critical curve for nitrogen-ammonia mixtures, N_2 (S. T. P.) per g. of NH_3 : ∇ , 100 cc.; \square , 150; \otimes , 200; \triangle , 250; \circ , 300.

was determined at 0° and at pressures to 1000 atmospheres. Over the same pressure range the solubility of nitrogen was measured at 0, 50, 75, 90 and 100° . Two critical points, one at 90° and about 600 atmospheres, the other at 100° and approximately 375 atmospheres, were found. The probable trend of the critical curve was sketched over a short range.

WASHINGTON, D. C.

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[CONTRIBUTION FROM THE CHEMICAL LABORATORY OF SMITH COLLEGE]

Thermodynamics of Lead Iodide¹

BY JESSIE Y. CANN AND ALICE C. TAYLOR

The purpose of this investigation is to determine, by means of electromotive force measurements, the free energy of formation, ΔF , the change of entropy, ΔS , and the change in heat content, ΔH , of lead iodide.

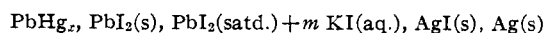
In contrast to some previous investigators, *e. g.*, Gerke² who used 1 and 0.1 *M* solutions of electrolytes, we have used 0.1, 0.05 and 0.025 *M*

(1) The experimental part of this paper is a portion of a thesis submitted by A. C. Taylor in partial fulfillment of the requirements for the degree of Master of Arts at Smith College.

(2) Gerke, *THIS JOURNAL*, **44**, 1684 (1922); and *Chem. Rev.*, **1**, 337 (1925).

solutions. Taylor³ and Taylor and Perrott⁴ have also studied lead iodide.

Method and Apparatus.—In this investigation the cell



was measured. Pyrex H-tubes were employed, similar to those used by Gerke.²

The cell was placed in the usual oil thermostat, regulated at 25° , and measurements were made

(3) Taylor, *THIS JOURNAL*, **38**, 2295 (1916).

(4) Taylor and Perrott, *ibid.*, **43**, 489 (1921).